CleanAir Project No. 13318 Revision 0, Final Report

APPENDIX B: SAMPLE CALCULATIONS

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# USEPA Method 5/29 (FPM/Metals) Sampling, Velocity and Moisture Sample Calculations

### Sample data taken from Run 1

Note: The tables presenting the results are generated electronically from raw data. It may not be possible to exactly duplicate these results using a calculator. The reference method data, results, and all calculations are carried to sixteen decimal places throughout. The final table is formatted to an appropriate number of significant figures.

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1. Volume of water collected (wscf)

$$V_{wstd} = (0.04706)(V_{lc})$$

Where:

 $V_{lc}$  = total volume of liquid collected in impingers and silica gel (ml) = 60.0 ml 0.04706 = ideal gas conversion factor (ft<sup>3</sup> water vapor/ml or gm) = 0.04706 ft<sup>3</sup>/ml  $V_{wstd}$  = volume of water vapor collected at standard conditions (ft<sup>3</sup>) = 2.82 ft<sup>3</sup>

2. Volume of gas metered, standard conditions (dscf)

$$V_{nextd} = \frac{(17.64)(V_m)(P_{bar} + \frac{\Delta H}{13.6})(Y_d)}{(460 + T_m)}$$

Where:

| $P_{bar}$  | = barometric pressure (in. Hg)   | = | 29.67  | in. Hg                     |
|------------|--|---|--------|----------------------------|
| $T_{m}$    | = average dry gas meter temperature (°F)   | = | 80.29  | °F                         |
| $V_{m}$    | <ul> <li>volume of gas sample through the dry gas meter at meter<br/>conditions (dcf)</li> </ul> | = | 34.48  | dcf                        |
| $Y_d$      | = gas meter correction factor (dimensionless)  | = | 0.9946 |                            |
| ΔΗ         | = average pressure drop across meter box orifice (in. H <sub>2</sub> O)                          | = | 0.97   | in. H <sub>2</sub> O       |
| 17.64      | = standard temperature to pressure ratio (°R/in. Hg)   | = | 17.64  | °R/in. Hg                  |
| 13.6       | = conversion factor (in. H₂O/in. Hg)   | = | 13.6   | in.H <sub>2</sub> O/in. Hg |
| 460        | = °F to °R conversion constant   | = | 460    |                            |
| $V_{mstd}$ | = volume of gas sampled through the dry gas meter at standard<br>conditions (dscf)               | = | 33.300 | dscf                       |

3. Sample gas pressure (in. Hg)

$$P_s = P_{bar} + \left(\frac{P_g}{13.6}\right)$$

Where:

| $P_{bar}$ | = barometric pressure (in. Hg)                      | = | 29.67 | in. Hg         |
|-----------|---|---|-------|----------------|
| $P_g$     | = sample gas static pressure (in. H <sub>2</sub> O) | = | -1.40 | in. H₂O        |
| 13.6      | = conversion factor (in. H₂O/in. Hg)                | = | 13.6  | in. H₂O/in. Hg |
|           |   |   |       |                |

 $P_s$  = absolute sample gas pressure (in. Hg) = 29.57 in. Hg

Defined

29.57

2.17

in. Hg

in. Hg

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4. Actual water vapor pressure at sample gas temperature less than 212°F (in. Hg)

|         | $\left(18.3036 - \frac{3816.44}{\frac{5}{9}(T_s - 32) + 273.15 - 46.13}\right)$ |
|---------|---|
| $P_v$ = | 25.4  |

| Where:         |   |   |         |              |
|----------------|---|---|---------|--------------|
| $T_s$          | = average sample gas temperature (°F)     | = | 104.00  | °F           |
| 18.3036        | = Antoine coefficient                     | = | 18.3036 | °K           |
| 3816.44        | = Antoine coefficient                     | = | 3816.44 | °K           |
| 273.15         | = temperature conversion factor           | = | 273.15  | °K           |
| 46.13          | = Antoine coefficient                     | = | 46.13   | °K           |
| 25.4           | = conversion factor                       | = | 25.4    | mm Hg/in. Hg |
| 5/9            | = Fahrenheit to Celsius conversion factor | = | 5/9     | °C/°F        |
| 32             | = temperature conversion (°F)             | = | 32      | °F           |
| P <sub>v</sub> | = vapor pressure, actual (in. Hg)         | = | 2.17    | in. Hg       |

5. Water vapor pressure at gas temperature greater than 212°F (in. Hg)

$$P_{v}$$
 =  $P_{s}$  Where: 
$$P_{s}$$
 = absolute sample gas pressure (in. Hg) = 29.57 in. Hg 
$$P_{v}$$
 = water vapor pressure, actual (in. Hg) = Previously in. Hg

6. Moisture measured in sample (% by volume)

$$B_{wo} = \frac{V_{wstd}}{\left(V_{mstd} + V_{wstd}\right)}$$
Where:
$$V_{mstd} = \text{volume of gas sampled through the dry gas meter at standard} = 33.300 dscf conditions (dscf)$$

$$V_{wstd} = \text{volume of water collected at standard conditions (scf)} = 2.82 scf$$

$$B_{wo} = \text{proportion of water measured in the gas stream by volume} = 0.0782 = 7.82 %$$

7. Saturated moisture content (% by volume)

$$B_{ws} = \frac{P_{v}}{P_{s}}$$
 Where:

 $P_{s} = \text{absolute sample gas pressure (in. Hg)}$ 
 $P_{v} = \text{water vapor pressure, actual (in. Hg)}$ 

 $\rm B_{ws}$  = proportion of water vapor in the gas stream by volume at \$0.0735\$ saturated conditions = 7.35 %

%

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8. Actual water vapor in gas (% by volume)

$$B_{w} = MINIMUM \left[ B_{wo}, B_{ws} \right]$$

Where:

 $B_{ws}$ = proportion of water vapor in the gas stream by volume at 0.0735

saturated conditions

 $B_{wo}$ = proportion of water measured in the gas stream by volume 0.0782

Bw = actual water vapor in gas 0.0735 7.35

9. Nitrogen (plus carbon monoxide) in gas stream (% by volume, dry)

$$N_2 + CO = 100 - CO_2 - O_2$$

Where:

CO2 = proportion of carbon dioxide in the gas stream by volume (%) 0.1 %

= proportion of oxygen in the gas stream by volume (%)  $O_2$ 21.0 % 100 = conversion factor (%) 100 %

N<sub>2</sub>+CO = proportion of nitrogen and CO in the gas stream by volume (%) 78.96

10. Molecular weight of dry gas stream (lb/lb·mole)

$$M_d = \left(M_{CO_2}\right) \frac{\left(CO_2\right)}{\left(100\right)} + \left(M_{O_2}\right) \frac{\left(O_2\right)}{\left(100\right)} + \left(M_{N_2 + CO}\right) \frac{\left(N_2 + CO\right)}{\left(100\right)}$$

Where:

 $M_{\text{CO2}}$ = molecular weight of carbon dioxide (lb/lb-mole) 44.00 lb/lb·mole  $M_{O2}$ = molecular weight of oxygen (lb/lb·mole) 32.00 lb/lb·mole M<sub>N2+CO</sub> = molecular weight of nitrogen and carbon monoxide (lb/lb·mole) 28.00 lb/lb-mole

CO2 = proportion of carbon dioxide in the gas stream by volume (%) 0.1 %  $O_2$ = proportion of oxygen in the gas stream by volume (%) 21.0 %

N<sub>2</sub>+CO = proportion of nitrogen and CO in the gas stream by volume (%) 79.0 % 100 = conversion factor (%) 100 %

 $M_d$ = dry molecular weight of sample gas (lb/lb·mole) 28.85 lb/lb-mole

11. Molecular weight of sample gas (lb/lb·mole)

$$M_s = (M_d)(1 - B_w) + (M_{H,O})(B_w)$$

Where:

= proportion of water vapor in the gas stream by volume 0.0735  $B_{\rm w}$ 

 $M_d$ = dry molecular weight of sample gas (lb/lb·mole) 28.85 ib/lb-mole  $M_{H2O}$ = molecular weight of water (lb/lb·mole) lb/lb·mole 18.00

Ms = molecular weight of sample gas, wet basis (lb/lb·mole) 28.05 lb/lb-mole

13,281

acfm

12. Velocity of sample gas (ft/sec)

| $V_s$ | $= (K_p)(C_P) \sqrt{\Delta P} \sqrt{\sqrt{\frac{T_s + 460}{(M_s)(P_s)}}}$ |
|-------|---|
|-------|---|

| Where: |   |   |        |            |
|--------|---|---|--------|------------|
| $K_p$  | = velocity pressure constant  | = | 85.49  |            |
| $C_p$  | = pitot tube coefficient  | = | 0.84   |            |
| $M_s$  | = wet molecular weight of sample gas, wet basis (lb/lb·mole)                  | = | 28.05  | lb/lb·mole |
| $P_s$  | = absolute sample gas pressure (in. Hg)                                       | = | 29.57  | in. Hg     |
| $T_s$  | = average sample gas temperature (°F)   | = | 104.00 | °F         |
| √∆P    | = average square roots of velocity heads of sample gas (in. H <sub>2</sub> O) | = | 0.815  | √in. H₂O   |
| 460    | = °F to °R conversion constant  | = | 460    |            |
| $V_s$  | = sample gas velocity (ft/sec)  | = | 48.26  | ft/sec     |

13. Volumetric flow rate of sample gas at actual gas conditions (acfm)

$$Q_a$$
 =  $(60)(A_s)(V_s)$  Where:

 $A_s$  = cross sectional area of sampling location (ft²) =  $4.59$  ft² 
 $V_s$  = sample gas velocity (ft/sec) =  $48.26$  ft/sec 
 $60$  conversion factor (sec/min) =  $60$  sec/min

= volumetric flow rate at actual conditions (acfm)

14. Total flow of sample gas (scfm)

$$Q_{s} = (Q_{a}) \left( \frac{P_{s}}{29.92} \right) \left( \frac{68 + 460}{T_{s} + 460} \right)$$

Where:

 $Q_a$ 

| $Q_a$ | <ul><li>volumetric flow rate at actual conditions (acfm)</li></ul> | = | 13,281 | acfm   |
|-------|--|---|--------|--------|
| $P_s$ | = absolute sample gas pressure (in. Hg)                            | = | 29.57  | in. Hg |
| 29.92 | = standard pressure (in. Hg)                                       | = | 29.92  | in. Hg |
| $T_s$ | = average sample gas temperature (°F)                              | = | 104.0  | °F     |
| 68    | = standard temperature (°F)  | = | 68     | °F     |
| 460   | = °F to °R conversion constant                                     | = | 460    |        |
| $Q_s$ | = volumetric flow rate at standard conditions, wet basis (scfm)    | = | 12,286 | scfm   |

15. Dry flow of sample gas (dscfm)

$$Q_{sud} = (Q_s)(1 - B_w)$$

Where:

 $B_w$  = proportion of water vapor in the gas stream by volume = 0.0735  $Q_s$  = volumetric flow rate at standard conditions, wet basis (scfm) = 12,286 scfm  $Q_{std}$  = volumetric flow rate at standard conditions, dry basis (dscfm) = 11,383 dscfm

16. Dry flow of sample gas corrected to 7%O<sub>2</sub> (dscfm)

$$Q_{std 7} = (Q_{std}) \left( \frac{20.9 - O_2}{20.9 - 7} \right)$$

Where:

| $Q_{std}$      | = volumetric flow rate at standard conditions, dry basis (dscfm) | = | 11,383 | dscfm |
|----------------|--|---|--------|-------|
| O <sub>2</sub> | = proportion of oxygen in the gas stream by volume (%)           | = | 21.0   | %     |
| 20.9           | = oxygen content of ambient air (%)                              | = | 20.9   | %     |
| 7              | = oxygen content of corrected gas (%)                            | = | 7.0    | %     |
|                |  |   |        |       |

 $Q_{\text{std7}}$  = volumetric flow rate at STP and 7%O<sub>2</sub>, dry basis (dscfm) = (52) dscfm

17. Hourly time basis conversion of volumetric flow rate ( $Q_{\text{std}}$  example)

$$Q_{std-hr} = (Q_{std-min})(60)$$

Where

| $Q_{\text{std-min}}$ | = volumetric flow rate, english units (ft³/min) | = | 11,383 | dscfm  |
|----------------------|---|---|--------|--------|
| 60                   | = conversion factor (min/hr)                    | = | 60     | min/hr |
|                      |   |   |        |        |

 $Q_{\text{std-hr}}$  = volumetric flow rate, hourly basis (dscf/hr) = 682,995 dscf/hr

18. Metric Conversion of Gas Volumes (Q<sub>std</sub> example)

$$Q_{std-metric} = \left(Q_{std-english}\right) \left(\frac{60}{35.31}\right)$$

Where:

| Q <sub>std-english</sub> | = volumetric flow rate, english units (ft³/min)        | = | 11,383 | dscfm                           |
|--------------------------|--|---|--------|---------------------------------|
| 35.31                    | = conversion factor (ft <sup>3</sup> /m <sup>3</sup> ) | = | 35.31  | ft <sup>3</sup> /m <sup>3</sup> |
| 60                       | = conversion factor (min/hr)                           | = | 60     | min/hr                          |

 $Q_{\text{std-metric}}$  = volumetric flow rate, metric units (m³/hr) = 19,343 dry std m³/hr

19. Standard to Normal Conversion of Gas Volumes (Q<sub>std</sub> example)

$$Q_{Normal} = \left(Q_{std-metric}\right) \left(\frac{32+460}{68+460}\right)$$

Where:

| Q <sub>std-metric</sub> | = volumetric flow rate, metric units (dry std m³/hr) | = | 19,343 | dry std m³/hr |
|-------------------------|--|---|--------|---------------|
| 32                      | = normal temperature (°F)                            | = | 32     | °F            |
| 68                      | standard temperature (°F)                            | = | 68     | °F            |
| 460                     | = standard temperature in Rankine (68°F)             | = | 460    |               |
|                         |  |   |        |               |

 $Q_{Normal}$  = volumetric flow rate, metric units (dry Nm<sup>3</sup>/hr) = 18,024 dry Nm<sup>3</sup>/hr

# 20. Percent isokinetic (%)

| 7      | $= (0.09450)(T_s + 460)(V_{mstd})$  |
|--------|---|
| 1      | $= \frac{1}{(P_s)(V_s)\left(\frac{(D_n)^2(\pi)}{(144)(4)}\right)(\Theta)(1-B_w)}$ |
| Where: |   |
| n      | - diameter of pozzla (in)   |

| Where:            |   |   |        |        |
|-------------------|---|---|--------|--------|
| D <sub>n</sub>    | = diameter of nozzle (in)   | = | 0.200  | in.    |
| $B_{w}$           | = proportion of water vapor in the gas stream by volume                           | = | 0.0735 |        |
| $P_s$             | = absolute sample gas pressure (in. Hg)   | = | 29.57  | in. Hg |
| Ts                | = average sample gas temperature (°F)   | = | 104.0  | °F     |
| V <sub>mstd</sub> | = volume of gas sample through the dry gas meter at standard<br>conditions (dscf) | = | 33.300 | dscf   |
| $V_s$             | = sample gas velocity (ft/sec)  | = | 48.26  | ft/sec |
| θ                 | = total sampling time (min)   | = | 60     | min    |
| 0.0945            | = conversion constant   | = | 0.0945 |        |
| 460               | = °F to °R conversion constant  | = | 460    |        |
|                   |   |   |        |        |
| 1                 | = percent of isokinetic sampling (%)  | = | 102.57 | %      |
|                   |   |   |        |        |

# 21. Alternative Method 5 Post-Test Meter Calibration Factor

| $Y_{qa}$<br>Where: | $= \frac{\Theta}{V_m} \sqrt{\frac{(0.0319)(T_m + 460)(28.96)}{(\Delta H_@)(P_{bar} + \frac{\Delta H}{13.6})(M_d)}} (\sqrt{\Delta H})_{avg}$ |   |        |                      |
|--------------------|---|---|--------|----------------------|
| θ                  | = total sampling time (min)   | = | 60     | min                  |
| $V_{m}$            | <ul> <li>volume of gas sample through the dry gas meter at meter<br/>conditions (dcf)</li> </ul>  | = | 34.48  | dcf                  |
| $T_{m}$            | = average dry gas meter temperature (°F)  | = | 80.29  | °F                   |
| $\Delta H_{@}$     | = dry gas meter orifice coefficient   | = | 1.7216 |                      |
| $P_{bar}$          | = barometric pressure (in. Hg)  | = | 29.67  | in. Hg               |
| $\Delta H$         | = average pressure drop across meter box orifice (in. H <sub>2</sub> O)   | = | 0.971  | in. H <sub>2</sub> O |
| $M_d$              | = dry molecular weight of sample gas (lb/lb·mole)   | = | 28.85  | lb/lb·mole           |
| √∆H <sub>avg</sub> | = average of square root of pressure drop across meter orifice  | = | 0.971  | √in. H₂O             |
| 0.0319             | = conversion constant   | = | 0.0319 |                      |
| 28.96              | = molecular weight of ambient air (lb/lb-mole)  | = | 28.96  | lb/lb-mole           |
| 13.6               | = conversion factor (in. H <sub>2</sub> O/in. Hg)   | = | 13.6   | in.H₂O/in. Hg        |
| 460                | = °F to °R conversion constant  | = | 460    |                      |

= alternative Method 5 post-test meter calibration factor

 $Y_{\mathsf{q}\mathsf{a}}$ 

0.9825

# USEPA Method 5 (FPM) Sample Laboratory Analysis Calculations for FPM

Sample data taken from Run 1

Note: The tables presenting the results are generated electronically from raw data. It may not be possible to exactly duplicate these results using a calculator. The reference method data, results, and all calculations are carried to sixteen decimal places throughout. The final table is formatted to an appropriate number of significant figures.

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### 1. Residue mass of filter used in calculation

|                      | or mital accumin containant        |   |   |         |   |
|----------------------|------------------------------------|---|---|---------|---|
| $m_{\it fi-calc}$    | $=m_{fi}$                          | if $m_{fi} \ge MDL_f$                     |   |         |   |
| $m_{\it fi-calc}$    | $= (MDL_f)(F_r)$                   | if $m_{fi} < MDL_f$                       |   |         |   |
| Where:               |                                    |   |   |         |   |
| m <sub>f1</sub>      | = reported mass of filter "1" from | m gravimetric analysis (g)                | = | 0.01240 | g |
| m <sub>f2</sub>      | = reported mass of filter "2" from | m gravimetric analysis (g)                | = |         | g |
| m <sub>f3</sub>      | = reported mass of filter "3" from | n gravimetric analysis (g)                | = |         | g |
| m <sub>f4</sub>      | = reported mass of filter "4" from | m gravimetric analysis (g)                | = |         | g |
| $MDL_f$              | = reported minimum gravimetri      | c detection limit for filter fraction (g) | = | 0.00010 | g |
| F <sub>r</sub>       | = fraction of MDL applied to not   | n-detectable run sample (g)               | = | 0.00    |   |
| m <sub>f1-calc</sub> | = residue mass of filter "1" used  | d in calculation (g)                      | = | 0.01240 | g |
| m <sub>f2-calc</sub> | = residue mass of filter "2" used  | d in calculation (g)                      | = |         | g |
| m <sub>f3-calc</sub> | = residue mass of filter "3" used  | d in calculation (g)                      | = |         | g |
| m <sub>f4-calc</sub> | = residue mass of filter "4" used  | d in calculation (g)                      | = |         | g |

### 2. Total filter residue (g)

$$m_{filter} = \sum_{i=1}^{n} m_{fi-calc}$$

### Where:

| m <sub>f1-calc</sub> | = residue mass of filter "1" used in calculation (g) | = | 0.01240 | g |
|----------------------|--|---|---------|---|
| m <sub>f2-calc</sub> | = residue mass of filter "2" used in calculation (g) | = |         | g |
| m <sub>f3-calc</sub> | = residue mass of filter "3" used in calculation (g) | = |         | g |
| m <sub>f4-calc</sub> | = residue mass of filter "4" used in calculation (g) | = |         | g |
|                      |  |   |         |   |
| m <sub>filter</sub>  | = total particulate collected on filters (g)         | = | 0.01240 | g |

3. Aliquot residue mass of blank sample used in calculation (g)

$$r_{ai-blank-calc}$$
 =  $r_{ai-blank}$  if  $r_{ai-blank} \ge MDL_s$   
 $r_{ai-blank-calc}$  =  $(MDL_s)(F_b)$  if  $r_{ai-blank} < MDL_s$ 

## Where:

|                            |  |   | Acetone |   |  |
|----------------------------|--|---|---------|---|--|
| r <sub>ai-blank</sub>      | = aliquot residue mass of blank sample for solvent "i" (g)                     | = | 0.00060 | g |  |
| MDLs                       | = reported minimum gravimetric detection limit for solvent rinse (g)           |   | 0.00010 | g |  |
| F₀                         | = fraction of MDL applied to non-detectable blank sample (g)                   | = | 0.00    |   |  |
|                            |  |   |         |   |  |
| r <sub>ai-blank-calc</sub> | = aliquot residue mass of blank sample for solvent "i" used in calculation (g) | = | 0.00060 | g |  |

4. Aliquot residue mass of run sample used in calculation (g)

$$r_{ai-calc} = r_{ai}$$
 if  $r_{ai} \ge MDL_s$   
 $r_{ai-calc} = (MDL_s)(F_r)$  if  $r_{ai} < MDL_s$ 

| Where:               |  |   | Acetone |   |
|----------------------|--|---|---------|---|
| $r_{ai}$             | = aliquot residue mass of run sample for solvent "i" (g)                     | = | 0.00780 | g |
| $MDL_s$              | = reported minimum gravimetric detection limit for solvent rinse (g)         | = | 0.00010 | g |
| F <sub>r</sub>       | = fraction of MDL applied to non-detectable run sample (g)                   | = | 1.00    |   |
| r <sub>ai-calc</sub> | = aliquot residue mass of run sample for solvent "i" used in calculation (g) | = | 0.00780 | g |

# 5. Residue mass of run sample (g)

$$r_{si} = \left(r_{ai-calc}\right) \left(\frac{v_{si}}{v_{ai}}\right)$$

| Where:<br>r <sub>ai-calc</sub> | = aliquot residue mass of run sample for solvent "i" used in calculation (g)      | = | Acetone<br>0.00780 | g  |
|--------------------------------|---|---|--------------------|----|
| V <sub>si</sub>                | = liquid volume of run sample for solvent rinse "i" (mL)                          | = | 136                | mL |
| V <sub>ai</sub>                | = aliquot volume use for solvent rinse "i" (mL) used in gravimetric analysis (mL) | = | 136                | mL |
| r                              | = residue mass of run sample for solvent rinse "i" (a)                            | _ | 0 00780            |    |

### 6. Maximum allowable blank correction for solvent rinse (g)

$$m_{bi} = MINIMUM \left[ \left( \frac{(r_{ai-blank-calc})(v_{si})}{v_{ai-blank}} \right) \text{ or } (0.00001)(\rho_i)(v_{si}) \text{ or } (r_{si}) \right]$$

| Where:                     |  |             | Acetone |      |
|----------------------------|--|-------------|---------|------|
| r <sub>ai-blank-calc</sub> | = blank aliquot residue mass for solvent "i" used in calculation (g) | <del></del> | 0.00060 | g    |
| $V_{si}$                   | = liquid volume of run sample for solvent rinse "i" (mL)             | =           | 136.0   | mL.  |
| V <sub>ai-blank</sub>      | = liquid volume of blank sample for solvent rinse "i" (mL)           | =           | 218.0   | mL   |
| 0.00001                    | = EPA M-5 fraction of total rinse that can be subtracted (g)         | =           | 0.00001 |      |
| $\rho_i$                   | = density of solvent rinse "i" (g/mL)                                | =           | 0.7845  | g/ml |
| r <sub>si</sub>            | = residue mass of run sample for solvent rinse "i" (g)               | =           | 0.00780 | g    |
|                            |  |             |         |      |
| $m_{bi}$                   | = maximum allowable blank correction for solvent rinse "i" (g)       | =           | 0.00037 | g    |

The first part of the expression is used for solvent rinse 1; the blank is the concentration of the blank, times the size of the sample

# 7. Net residue mass of run sample (g)

$$m_i = (r_{si} - m_{bi})$$

| Where:          |  |   | Acetone |   |
|-----------------|--|---|---------|---|
| r <sub>si</sub> | = residue mass of run sample for solvent rinse "i" (g)         | = | 0.00780 | g |
| $m_{bi}$        | = maximum allowable blank correction for solvent rinse "i" (g) | = | 0.00037 | g |
| m <sub>i</sub>  | = net residue mass of run sample for solvent rinse "i" (g)     | = | 0.00743 | g |

## 8. Total solvent residue - (g)

$$m_s = \sum_{i=1}^n m_i$$

# Where:

| m <sub>1</sub> | = net residue mass of solvent rinse "1" (g) | = | 0.00743 | g |
|----------------|---|---|---------|---|
| m <sub>2</sub> | = net residue mass of solvent rinse "2" (g) | = | N/A     | g |
| m <sub>3</sub> | = net residue mass of solvent rinse "3" (g) | = | N/A     | g |
| m <sub>s</sub> | = total solvent residue (g)                 | = | 0.00743 | g |

# 9. Total gravimetric result (g)

$$m_T = m_{filter} + m_s$$

## Where:

| m <sub>filter</sub> | = total particulate collected on filters (g) | = | 0.01240 | g |
|---------------------|--|---|---------|---|
| $m_s$               | = total solvent residue (g)                  | = | 0.00743 | g |
| m <sub>T</sub>      | = total gravimetric result (g)               | = | 0.01983 | q |

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10. Total gravimetric detection limit (g)

$$m_D = (MDL_f)(n_f) + (MDL_s)(n_s)$$

Where:

| vviicie.       |  |   |         |   |
|----------------|--|---|---------|---|
| $MDL_f$        | = reported minimum gravimetric detection limit for filter fraction (g) | = | 0.00010 | g |
| n <sub>f</sub> | = number of filters in analysis  | = | 1       |   |
| MDLs           | = reported minimum gravimetric detection limit for solvent rinse (g)   | = | 0.00010 | g |
| $n_s$          | = number of solvent rinses in analysis                                 | = | 1       |   |
|                |  |   |         |   |

 $m_{\text{D}}$ = total gravimetric detection limit (g) = 0.00020 g

11. Total filterable particulate matter (g)

$$m_n = MAXIMUM[m_T \ or \ m_D]$$

Where:

 $m_{n} \\$ 

= total gravimetric result (g) = 0.01983 g  $m_{\text{T}} \\$ = total gravimetric detection limit (g) 0.00020 g  $m_{\text{\tiny D}}$ = total filterable particulate matter (g) = 0.01983 g

# USEPA Method 5 (FPM) Sample Emission Calculations for FPM

### Sample data taken from Run 1

Note: The tables presenting the results are generated electronically from raw data. It may not be possible to exactly duplicate these results using a calculator. The reference method data, results, and all calculations are carried to sixteen decimal places throughout. The final table is formatted to an appropriate number of significant figures.

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1. Filterable particulate matter concentration (lb/dscf)

$$C_{sd} = \left(\frac{m_n}{V_{mstd}}\right) \left(2.205 \times 10^{-3}\right)$$

Where:

 $m_n$  = total filterable particulate matter (g) = 0.01983 g  $V_{matd}$  = volume metered, standard (dscf) = 33.3002 dscf  $2.205 \times 10^{-3}$  = conversion factor (lb/g) = 2.205E-03 lb/g

C<sub>sd</sub> = filterable particulate matter concentration (lb/dscf) = 1.3128E-06 lb/dscf

2. Filterable particulate matter concentration (gr/dscf)

$$C_{sd} = \left(\frac{m_n}{V_{mstd}}\right) (15.43)$$

Where:

 $m_n$  = total filterable particulate matter (g) = 0.01983 g  $V_{mstd}$  = volume metered, standard (dscf) = 33.3002 dscf 15.43 = conversion factor (gr/g) = 15.43 gr/g

 $C_{sd}$  = filterable particulate matter concentration (gr/dscf) = 0.0092 gr/dscf

3. Filterable particulate matter concentration (mg/dscm)

$$C_{sd} = \left(\frac{m_n}{V_{mstd}}\right) (1000)(35.31)$$

Where:

 $m_n$ = total filterable particulate matter (g)= 0.01983g $V_{mstd}$ = volume metered, standard (dscf)= 33.3002dscf1000= conversion factor (mg/g)= 1000mg/g35.31= conversion factor (dscf/dscm)= 35.31dscf/dscm

C<sub>sd</sub> = filterable particulate matter concentration (mg/dscm) = 21.0222 mg/dscm

4. Filterable particulate matter concentration (mg/Nm3 dry)

$$C_{sd}$$
 =  $\left(\frac{m_n}{V_{mstd}}\right) (1000)(35.31) \left(\frac{68+460}{32+460}\right)$ 

Where:

 $m_n$ = total filterable particulate matter (g) 0.01983  $V_{\text{mstd}}$ = volume metered, standard (dscf) 33.3002 1000 = conversion factor (mg/g) 1000 mg/g 35.31 = conversion factor (dscf/dscm) 35.31 dscf/dscm 68 = standard temperature (°F) ۰F 68 32 = normal temperature (°F) 32 ۰F 460 = °F to °R conversion constant 460

 $C_{sd}$  = filterable particulate matter concentration (mg/Nm3 dry) = 22.5604 mg/Nm<sup>3</sup> dry

0.0079

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5. Filterable particulate matter concentration at actual gas conditions (gr/acf example)

$$C_a = C_{sd} \left( \frac{Q_{std}}{Q_a} \right)$$

|           | ( - " )  |   |        |         |
|-----------|--|---|--------|---------|
| Where:    |  |   |        |         |
| $C_{sd}$  | = filterable particulate matter concentration (gr/dscf)          | = | 0.0092 | gr/dscf |
| $Q_{std}$ | = volumetric flow rate at standard conditions, dry basis (dscfm) | = | 11,383 | dscfm   |
| $Q_a$     | = volumetric flow rate at actual conditions (acfm)               | = | 13,281 | acfm    |
|           |  |   |        |         |

= filterable particulate matter concentration at actual gas conditions (gr/acf)

6. Filterable particulate matter rate (lb/hr)

$$E_{lb/hr} = \left(\frac{m_n}{V_{mstd}}\right) (2.205 \times 10^{-3}) (Q_{std}) (60)$$

Where:

 $C_{\mathsf{a}}$ 

| m <sub>n</sub>           | = total filterable particulate matter (g)                        | = | 0.01983   | g      |
|--------------------------|--|---|-----------|--------|
| $V_{mstd}$               | = volume metered, standard (dscf)                                | = | 33.3002   | dscf   |
| 2.205 x 10 <sup>-3</sup> | = conversion factor (lb/g)                                       | = | 2.205E-03 | lb/g   |
| $Q_{std}$                | = volumetric flow rate at standard conditions, dry basis (dscfm) | = | 11,383    | dscfm  |
| 60                       | = conversion factor (min/hr)                                     | = | 60        | min/hr |
| _                        |  |   |           |        |
| E <sub>lb/hr</sub>       | = filterable particulate matter rate (lb/hr)                     | = | 0.8966    | lb/hr  |

7. Filterable particulate matter rate (kg/hr)

$$E_{kg/hr} = \left(\frac{m_n}{V_{mstd}}\right) \left(\frac{Q_{std}}{1000}\right)$$

| Where:             |  |   |         |        |
|--------------------|--|---|---------|--------|
| m <sub>n</sub>     | = total filterable particulate matter (g)                        | = | 0.01983 | g      |
| $V_{mstd}$         | = volume metered, standard (dscf)                                | = | 33.3002 | dscf   |
| $Q_{std}$          | = volumetric flow rate at standard conditions, dry basis (dscfm) | = | 11,383  | dscfm  |
| 60                 | = conversion factor (min/hr)                                     | = | 60      | min/hr |
| 1000               | = conversion factor (g/kg)                                       | = | 1000    | g/kg   |
| E <sub>kg/hr</sub> | = filterable particulate matter rate (kg/hr)                     | = | 0.4066  | kg/hr  |

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8. Filterable particulate matter rate - Production-based (lb/tons of feed)

$$E_{Rp} = \left(\frac{m_n}{V_{mstd}}\right) \left(2.205 \times 10^{-3}\right) \left(\frac{(Q_{std})(60)}{R_p}\right)$$

Where:

| m <sub>n</sub>           | = total filterable particulate matter (g)                        | = | 0.01983   | g               |
|--------------------------|--|---|-----------|-----------------|
| $V_{mstd}$               | = volume metered, standard (dscf)                                | = | 33.3002   | dscf            |
| 2.205 x 10 <sup>-3</sup> | = conversion factor (lb/g)                                       | = | 2.205E-03 | lb/g            |
| $Q_{std}$                | = volumetric flow rate at standard conditions, dry basis (dscfm) | = | 11,383    | dscfm           |
| 60                       | = conversion factor (min/hr)                                     | = | 60        | min/hr          |
| $R_p$                    | = production rate (tons of feed/hr)                              | = | 323       | tons of feed/hr |

E<sub>Rp</sub> = filterable particulate matter rate - production-based (lb/tons of feed) = 0.00278 lb/tons of feed

9. Filterable particulate matter rate - Production-based (kg/tons of feed)

$$E_{Rp} = \left(\frac{m_n}{V_{mstd}}\right) \left(\frac{(Q_{std})(60)}{(1000)(R_p)}\right)$$

Where:

| m <sub>n</sub> | = total filterable particulate matter (g)                        | = | 0.01983 | g               |
|----------------|--|---|---------|-----------------|
| $V_{mstd}$     | = volume metered, standard (dscf)                                | = | 33.3002 | dscf            |
| 1000           | = conversion factor (g/kg)                                       | = | 1000    | g/kg            |
| $Q_{std}$      | = volumetric flow rate at standard conditions, dry basis (dscfm) | = | 11,383  | dscfm           |
| 60             | = conversion factor (min/hr)                                     | = | 60      | min/hr          |
| $R_p$          | = production rate (tons of feed/hr)                              | = | 323     | tons of feed/hr |

 $E_{Rp}$  = filterable particulate matter rate - production-based (kg/tons of feed) = 0.00126 kg/tons of feed

# LOGIC FOR TREATING DETECTION LIMITS

(mercury only)

# 1. Logic for Determining Total Blank (m<sub>Total-B</sub>) from 5 Fractions

|         | CASE 1 All 5 fractions are D. | CASE 2<br>1 to 4 fractions are ND | CASE 3 All 5 fractions are ND        |
|---------|-------------------------------|-----------------------------------|--------------------------------------|
| Rule    |                               |                                   |                                      |
| ND = 0  | $m_{Total-B} = Sum D, 1-5$    | $m_{Total-B} = Sum D$             | $m_{Total-B} = < Sum ND$             |
| ND=1x   | $m_{Total-B} = Sum D, 1-5$    | $m_{Total-B} = Sum D$             | $m_{Total-B} = < Sum ND$             |
| ND=0.5x | $m_{Total-B} = Sum D, 1-5$    | $m_{Total-B} = Sum D$             | $m_{Total-B} = < 0.5 \text{ Sum ND}$ |

# 2. Logic for Determining Total Sample (m<sub>Total-S</sub>) from 5 Fractions

|         | CASE 1 All 5 fractions are D.     | CASE 2<br>1 to 4 fractions are ND        | CASE 3 All 5 fractions are ND        |
|---------|-----------------------------------|--|--------------------------------------|
| Rule    |                                   |  |                                      |
| ND = 0  | m <sub>Total-S</sub> = Sum D, 1-5 | $m_{Total-S} = Sum D$                    | $m_{Total-S} = < Sum ND$             |
| ND=1x   | $m_{Total-S} = Sum D, 1-5$        | $m_{Total-S} = < [Sum D + Sum ND]$       | $m_{Total-S} = < Sum ND$             |
| ND=0.5x | $m_{Total-S}$ = Sum D, 1-5        | m <sub>Total-S</sub> = < [SumD+0.5 SumND | $m_{Total-S} = < 0.5 \text{ Sum ND}$ |

# 3. Logic for Determining Maximum Allowable Blank Correction (m<sub>T-B-allow</sub>)

|         | CASE 1 All 5 fractions are D. m <sub>Total-B</sub> = D | CASE 2 1 to 4 sample fractions are ND m <sub>Total-B</sub> = D |                     | CASE 4 Any type of fractions m <sub>Total-B</sub> = ND |
|---------|--|--|---------------------|--|
| Rule    |  |  |                     |  |
| ND = 0  | $m_{T-B-allow} = M29 Rule$                             | m <sub>T-B-allow</sub> = M29 Rule                              | $m_{T-B-allow} = 0$ | $m_{T-B-allow} = 0$                                    |
| ND=1x   | $m_{T-B-allow} = M29 Rule$                             | m <sub>T-B-allow</sub> = M29 Rule <sup>*</sup>                 | $m_{T-B-allow} = 0$ | $m_{T-B-allow} = 0$                                    |
| ND=0.5x | $m_{T-B-allow} = M29 Rule$                             | m <sub>T-B-allow</sub> = M29 Rule <sup>*</sup>                 | $m_{T-B-allow} = 0$ | $m_{T-B-allow} = 0$                                    |

<sup>\*</sup> M29 rule using only detected sample quantities for logical comparisons.

### 4. Logic for Determining Blank-Corrected Sample Amount (m<sub>n</sub>)

|                                 | CASE 1<br>All 5 fractions are D.<br>$m_{Total-S}$ - $m_{T-B-allow} \ge MIN(MDL)$                                  | CASE 2<br>1 to 4 sample fractions are ND $m_{Total-S}$ - $m_{T-B-allow} \ge MIN(MDL)$  |   | CASE 4 Any type of fractions m <sub>Total-S</sub> - m <sub>T-B-allow</sub> < MIN(MDL) |
|---------------------------------|---|--|---|---|
| Rule $ND = 0$ $ND=1x$ $ND=0.5x$ | $m_n = m_{Total-S} - m_{T-B-allow}$<br>$m_n = m_{Total-S} - m_{T-B-allow}$<br>$m_n = m_{Total-S} - m_{T-B-allow}$ | $\begin{split} m_n &= m_{\text{Total-S}} - m_{\text{T-B-allow}} \\ m_n &= < [m_{\text{Total-S}} - m_{\text{T-B-allow}}] \\ m_n &= < [m_{\text{Total-S}} - m_{\text{T-B-allow}}] \end{split}$ | $\begin{split} m_n &= < m_{\text{Total-S}} \\ m_n &= < m_{\text{Total-S}} \\ m_n &= < m_{\text{Total-S}} \end{split}$ | $m_n = \langle MIN[MDL]$<br>$m_n = \langle MIN[MDL]$<br>$m_n = \langle MIN[MDL]$      |

### **Definitions and Notes**

The term "Rule" refers to the rule being implemented for handling non-detectable quantities in summations.

MDL = minimum detection limit.

D = Detectable quantity reported as D.

ND = Non-Detectable quantity reported at a value of ND.

MIN[MDL] = lowest quantity of all detection limits for 5 fractions.

# USEPA Method 5/29 (FPM/Metals) Mercury Analyte Calculations

### Sample data taken from Run 1

Note: The tables presenting the results are generated electronically from raw data. It may not be possible to exactly duplicate these results using a calculator. The reference method data, results, and all calculations are carried to sixteen decimal places throughout. The final table is formatted to an appropriate number of significant figures.

Note: Please see the preceding page concerning treatment of minimum detection limits and mathematical operations on values that are below minimum detection limits.

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### 1. Total blank amount (µg)

$$m_{total-B} = \sum_{i=1}^{n} m_{i-B}$$

| Where:              |   |   |         |    |
|---------------------|---|---|---------|----|
| m <sub>1b-B</sub>   | = mercury amount in blank for Fraction 1b | = | <0.1000 | μg |
| m <sub>2b-B</sub>   | = mercury amount in blank for Fraction 2b | = | <0.2000 | μg |
| m <sub>3a-B</sub>   | = mercury amount in blank for Fraction 3a | = | <0.2000 | μg |
| m <sub>3b-B</sub>   | = mercury amount in blank for Fraction 3b | = | <0.5000 | μg |
| m <sub>3c-B</sub>   | = mercury amount in blank for Fraction 3c | = | <0.4000 | μg |
|                     | - botal and one of a constant to be all   | _ | -1 1000 |    |
| $m_{total	ext{-B}}$ | = total amount of mercury in blank        | = | <1.4000 | μg |

### 2. Total sample amount (µg)

$$m_{total - S}$$
 =  $\sum_{i=1}^{n} m_{i-S}$ 

| Where:            |  |   |         |    |
|-------------------|--|---|---------|----|
| m <sub>1b-S</sub> | = mercury amount in sample for Fraction 1b | = | <0.1000 | μg |
| m <sub>2b-S</sub> | = mercury amount in sample for Fraction 2b | = | <0.4000 | μg |
| m <sub>3a-S</sub> | = mercury amount in sample for Fraction 3a | = | <0.2000 | μg |
| m <sub>3b-S</sub> | = mercury amount in sample for Fraction 3b | = | 11.4605 | μg |
| m <sub>3c-S</sub> | = mercury amount in sample for Fraction 3c | = | 19.3802 | μg |
| Mtotal-S          | = total amount of mercury in sample        | = | 30.8407 | μα |

# 3. Allowable blank correction (µg)

$$m_{T-B-allow} = m_{total-B} \text{ if } m_{total-B} \le 0.6$$
 $m_{T-B-allow} = MAX \left[ 0.6, MIN \left( m_{total-B}, 0.05 \times m_{total-S} \right) \right] \text{ if } m_{total-B} > 0.6$ 

## Where:

| m <sub>total-B</sub>      | = total amount of mercury in blank  | = | <1.4000 | μg |
|---------------------------|-------------------------------------|---|---------|----|
| m <sub>total-S</sub>      | = total amount of mercury in sample | = | 30.8407 | μg |
| $0.05 \times m_{total-S}$ | = 5% of $m_{total-S}$               | = | 1.5420  | μg |

MAX = arithmetic operator that returns the maximum of two values

MIN = arithmetic operator that returns the minimum of two values

 $m_{T-B-allow}$  = total allowable blank correction = 0.0000 µg

NOTE: In this case, the second criteria applies.

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# 4. Sample corrected for allowable blank - Total (µg)

$$m_n = m_{total-S} - m_{T-B-allow}$$

Where:

| m <sub>total-S</sub>   | = total amount of mercury in sample | = | 30.8407 | μg |
|------------------------|-------------------------------------|---|---------|----|
| m <sub>T-B-allow</sub> | = total allowable blank correction  | = | 0.0000  | μg |
|                        |                                     |   |         |    |

 $m_n$  = total mercury in sample corrected for allowable blank = 30.8407  $\mu g$ 

# 5. Sample corrected for allowable blank - Prorated for each fraction ( $\mu g$ )

$$m_{n-i} = \left(\frac{m_{i-S}}{m_{total-S}}\right) (m_n)$$

| W  | ha | ro. |
|----|----|-----|
| VV |    | ш.  |

| VVIIGIG.             |  |   |         |    |
|----------------------|--|---|---------|----|
| m <sub>n</sub>       | = total mercury in sample corrected for allowable blank  | = | 30.8407 | μg |
| m <sub>1b-S</sub>    | = mercury amount in sample for Fraction 1b               | = | <0.1000 | μg |
| m <sub>2b-S</sub>    | = mercury amount in sample for Fraction 2b               | = | <0.4000 | μg |
| m <sub>3a-S</sub>    | = mercury amount in sample for Fraction 3a               | = | <0.2000 | μg |
| m <sub>3b-S</sub>    | = mercury amount in sample for Fraction 3b               | = | 11.4605 | μg |
| m <sub>3c-S</sub>    | = mercury amount in sample for Fraction 3c               | = | 19.3802 | μg |
| m <sub>total-S</sub> | = total amount of mercury in sample                      | = | 30.8407 | μg |
| m <sub>n-1b</sub>    | = mercury corrected for blank - prorated for Fraction 1b | = | <0.1000 | μg |
| m <sub>n-2b</sub>    | = mercury corrected for blank - prorated for Fraction 2b | = | <0.4000 | μg |
| m <sub>n-3a</sub>    | = mercury corrected for blank - prorated for Fraction 3a | = | <0.2000 | μg |
| m <sub>n-3b</sub>    | = mercury corrected for blank - prorated for Fraction 3b | = | 11.4605 | μg |
| m <sub>n-3c</sub>    | = mercury corrected for blank - prorated for Fraction 3c | = | 19.3802 | μg |
|                      |  |   |         |    |

# USEPA Method 5/29 (FPM/Metals) Mercury Sample Calculations

### Sample data taken from Run 1

Note: The tables presenting the results are generated electronically from raw data. It may not be possible to exactly duplicate these results using a calculator. The reference method data, results, and all calculations are carried to sixteen decimal places throughout. The final table is formatted to an appropriate number of significant figures.

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1. Mercury concentration (lb/dscf)

$$C_{sd} = \left(\frac{m_n}{V_{mstd}}\right) \left(\frac{2.205 \times 10^{-3}}{10^6}\right)$$

Where:

 $m_n$  = mercury collected in sample (total μg) = 30.8407 μg  $V_{mstd}$  = volume metered, standard (dscf) = 33.3002 dscf  $2.205 \times 10^{-3}$  = conversion factor (lb/g) = 2.205E-03 lb/g  $10^6$  = conversion factor (μg/g) = 1.0E+06 μg/g

 $C_{sd}$  = mercury concentration (lb/dscf) = 2.0421E-09 lb/dscf

2. Mercury concentration (µg/dscm)

$$C_{sd} = \left(\frac{m_n}{V_{mstd}}\right) (35.31)$$

Where:

 $m_n$  = mercury collected in sample (total μg) = 30.8407 μg  $V_{mstd}$  = volume metered, standard (dscf) = 33.3002 dscf 35.31 = conversion factor (dscf/dscm) = 35.31 dscf/dscm

 $C_{sd}$  = mercury concentration (µg/dscm) = 3.2702E+01 µg/dscm

3. Mercury concentration (mg/dscm)

$$C_{sd} = \left(\frac{m_n}{V_{mstd}}\right) \left(\frac{35.31}{1000}\right)$$

Where:

= mercury collected in sample (total µg) 30.8407  $m_n$ μg 33.3002 = volume metered, standard (dscf)  $V_{mstd}$ dscf = conversion factor (dscf/dscm) 35.31 dscf/dscm 35.31 1000 = conversion factor (µg/mg) 1000 μg/mg

 $C_{sd}$  = mercury concentration (mg/dscm) = 3.2702E-02 mg/dscm

# **4.** Mercury concentration (μg/Nm3 dry)

$$C_{sd} = \left(\frac{m_n}{V_{mstd}}\right) (35.31) \left(\frac{68 + 460}{32 + 460}\right).$$

# Where:

| $m_n$      | = mercury collected in sample (total µg) | = | 30.8407 | μg        |
|------------|--|---|---------|-----------|
| $V_{mstd}$ | = volume metered, standard (dscf)        | = | 33.3002 | dscf      |
| 35.31      | = conversion factor (dscf/dscm)          | = | 35.31   | dscf/dscm |
| 68         | = standard temperature (°F)              | = | 68      | °F        |
| 32         | = normal temperature (°F)                | = | 32      | °F        |
| 460        | = °F to °R conversion constant           | = | 460     |           |
|            |  |   |         |           |

 $C_{sd}$  = mercury concentration (µg/Nm3 dry) = 3.5095E+01 µg/Nm<sup>3</sup> dry

# 5. Mercury concentration at actual gas conditions (lb/acf example)

$$C_a = C_{sd} \left( \frac{Q_{std}}{Q_a} \right)$$

### Where:

| $C_{sd}$  | = mercury concentration (lb/dscf)                                | = | 2.0421E-09 | lb/dscf |
|-----------|--|---|------------|---------|
| $Q_{std}$ | = volumetric flow rate at standard conditions, dry basis (dscfm) | = | 11,383     | dscfm   |
| $Q_a$     | = volumetric flow rate at actual conditions (acfm)               | = | 13,281     | acfm    |
|           |  |   |            |         |

C<sub>a</sub> = mercury concentration at actual gas conditions (lb/acf) = 1.7504E-09 lb/acf

# 6. Mercury emission rate (lb/hr)

$$E_{lb/hr} = \left(\frac{m_n}{V_{mstd}}\right) \left(\frac{2.205 \times 10^{-3}}{10^6}\right) (Q_{std}) (60)$$

## Where:

| $m_n$                    | = mercury collected in sample (total µg)                         | = | 30.8407   | μg     |
|--------------------------|--|---|-----------|--------|
| $V_{mstd}$               | = volume metered, standard (dscf)                                | = | 33.3002   | dscf   |
| 2.205 x 10 <sup>-3</sup> | = conversion factor (lb/g)                                       | = | 2.205E-03 | lb/g   |
| 10 <sup>6</sup>          | = conversion factor (µg/g)                                       | = | 1.0E+06   | μg/g   |
| $Q_{std}$                | = volumetric flow rate at standard conditions, dry basis (dscfm) | = | 11,383    | dscfm  |
| 60                       | = conversion factor (min/hr)                                     | = | 60        | min/hr |

 $E_{lb/hr}$  = mercury emission rate (lb/hr) = 1.3948E-03 lb/hr

### 7. Mercury emission rate (g/s)

$$E_{g/s} = \left(\frac{m_n}{V_{mstd}}\right) \left(\frac{Q_{std}}{(10^6)(60)}\right)$$

### Where:

| $m_n$           | = mercury collected in sample (total μg)                         | = | 30.8407 | μg      |
|-----------------|--|---|---------|---------|
| $V_{mstd}$      | = volume metered, standard (dscf)                                | = | 33.3002 | dscf    |
| $Q_{std}$       | = volumetric flow rate at standard conditions, dry basis (dscfm) | = | 11,383  | dscfm   |
| 10 <sup>6</sup> | = conversion factor (μg/g)                                       | = | 1.0E+06 | µg/g    |
| 60              | = conversion factor (sec/min)                                    | = | 60      | sec/min |

 $E_{g/s}$  = mercury emission rate (g/s) = 1.7571E-04 g/s

# 8. Mercury Emission Rate - Production-based (lb/unit)

$$E_{RP} = \left(\frac{m_n}{V_{mstd}}\right) \left(\frac{2.205 \times 10^{-3}}{10^6}\right) \left(\frac{(Q_{std})(60)}{R_p}\right)$$

### Where:

| $m_n$                    | = mercury collected in sample (total μg)                         | = | 30.8407   | μg         |
|--------------------------|--|---|-----------|------------|
| $V_{mstd}$               | = volume metered, standard (dscf)                                | = | 33.3002   | dscf       |
| 2.205 x 10 <sup>-3</sup> | = conversion factor (lb/g)                                       | = | 2.205E-03 | lb/g       |
| 10 <sup>6</sup>          | = conversion factor (µg/g)                                       | = | 1.0E+06   | μg/g       |
| $Q_{std}$                | = volumetric flow rate at standard conditions, dry basis (dscfm) | = | 11,383    | dscfm      |
| 60                       | = conversion factor (min/hr)                                     | = | 60        | min/hr     |
| $R_p$                    | = production rate (units/hr)                                     | = | 323       | units/hour |
|                          |  |   |           |            |

 $E_{RP}$  = mercury emission rate - production-based (lb/xxxxx) = 4.3176E-06 lb/unit

# 9. Mercury Emission Rate - Production-based (g/unit)

$$E_{RP} = \left(\frac{m_n}{V_{mstd}}\right) \left(\frac{(Q_{std})(60)}{(10^6)(R_p)}\right)$$

### Where:

| $m_n$           | = mercury collected in sample (total μg)                         | = | 30.8407 | μg         |
|-----------------|--|---|---------|------------|
| $V_{mstd}$      | = volume metered, standard (dscf)                                | = | 33.3002 | dscf       |
| 10 <sup>6</sup> | = conversion factor (μg/g)                                       | = | 1.0E+06 | μg/g       |
| $Q_{std}$       | = volumetric flow rate at standard conditions, dry basis (dscfm) | = | 11,383  | dscfm      |
| 60              | = conversion factor (min/hr)                                     | = | 60      | min/hr     |
| R <sub>p</sub>  | = production rate (units/hr)                                     | = | 323     | units/hour |

E<sub>RP</sub> = mercury emission rate - production-based (g/xxxxx) = 1.9581E-03 g/unit

# LOGIC FOR TREATING DETECTION LIMITS

(all metals except mercury)

### 1. Logic for Determining Maximum Allowable Front-Half Blank Correction (m<sub>FB-allow</sub>)

|         | CASE 1                           | CASE 2             |
|---------|----------------------------------|--------------------|
|         | $m_{FB} = D$                     | $m_{FB} = ND$      |
| Rule    |                                  |                    |
| ND = 0  | $m_{FB-allow} = M29 Rule$        | $m_{FB-allow} = 0$ |
| ND=1x   | m <sub>FB-allow</sub> = M29 Rule | $m_{FB-allow} = 0$ |
| ND=0.5x | m <sub>FB-allow</sub> = M29 Rule | $m_{FB-allow} = 0$ |

# 2. Logic for Determining Blank-Corrected Front-Half Sample Amount (m<sub>F</sub>)

|         | CASE 1<br>$m_{FS}$ - $m_{FB\text{-allow}} \ge MDL$ | CASE 2<br>m <sub>FS</sub> - m <sub>FB-allow</sub> < MDL |
|---------|--|---|
| Rule    |  |   |
| ND = 0  | $m_F = m_{FS} - m_{FB-allow}$                      | $m_F = < MDL$   |
| ND=1x   | $m_F = m_{FS} - m_{FB-allow}$                      | $m_F = < MDL$   |
| ND=0.5x | $m_F = m_{FS} - m_{FB-allow}$                      | $m_F = < MDL$   |
|         |  |   |

# 3. Logic for Determining Maximum Allowable Back-Half Blank Correction (m<sub>BB-allow</sub>)

|         | CASE 1                           | CASE 2             |
|---------|----------------------------------|--------------------|
|         | $m_{BB} = D$                     | $m_{BB} = ND$      |
| Rule    |                                  |                    |
| ND = 0  | $m_{BB-allow} = M29 Rule$        | $m_{BB-allow} = 0$ |
| ND=1x   | $m_{BB-allow} = M29 Rule$        | $m_{BB-allow} = 0$ |
| ND=0.5x | m <sub>BB-allow</sub> = M29 Rule | $m_{BB-allow} = 0$ |

### 4. Logic for Determining Blank-Corrected Back-Half Sample Amount (m<sub>B</sub>)

|         | CASE 1                            | CASE 2                          |
|---------|-----------------------------------|---------------------------------|
|         | $m_{BS}$ - $m_{BB-allow} \ge MDL$ | $m_{BS}$ - $m_{BB-allow}$ < MDL |
| Rule    |                                   |                                 |
|         |                                   | 1 1 1 1 1                       |
| ND = 0  | $m_B = m_{BS} - m_{BB-allow}$     | $m_B = < MDL$                   |
| ND=1x   | $m_B = m_{BS} - m_{BB-allow}$     | $m_B = < MDL$                   |
| ND=0.5x | $m_B = m_{BS} - m_{BB-allow}$     | $m_B = < MDL$                   |

# 5. Logic for Adding Front and Back-Half Corrected Samples (m<sub>n</sub>)

|         | CASE 1<br>Both are D | CASE 2 One is D, other is ND     | CASE 3 Both are ND           |
|---------|----------------------|----------------------------------|------------------------------|
| Rule    |                      |                                  |                              |
| ND = 0  | $m_n = m_F + m_B$    | $m_n = D$                        | $m_n = < Sum ND$             |
| ND=1x   | $m_n = m_F + m_B$    | $m_n = \langle [D + ND] \rangle$ | $m_n = < Sum ND$             |
| ND=0.5x | $m_p = m_E + m_B$    | $m_p = < [D + 0.5ND]$            | $m_n = < 0.5 \text{ Sum ND}$ |

# **Definitions and Notes**

The term "Rule" refers to the rule being implemented for hanMDLing non-detectable quantities in summations MDL = minimum detection limit.

D = Detectable quantity reported as D.

ND = Non-Detectable quantity reported at a value of ND.

If Front and Back-Half fractions are combined, then only Items 1 and 2 are used.

SS Metals-1 Version 2006-12c

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# USEPA Method 5/29 (FPM/Metals) Phosphorus Analyte Calculations

### Sample data taken from Run 1

Note: The tables presenting the results are generated electronically from raw data. It may not be possible to exactly duplicate these results using a calculator. The reference method data, results, and all calculations are carried to sixteen decimal places throughout. The final table is formatted to an appropriate number of significant figures.

Note: Please see the preceding page concerning treatment of minimum detection limits and mathematical operations on values that are below minimum detection limits.

101017 121303

1. Maximum front-half blank correction criteria (µg)

$$A = (1.4) \left(\frac{3.141593}{4}\right) \left(\frac{D}{2.54}\right)^2$$

| W  | ha | ro. |
|----|----|-----|
| VV | nΘ | LG. |

| D        | = diameter of filter used in sample apparatus    | = | 8.2      | cm     |
|----------|--|---|----------|--------|
| 1.4      | = allowable blank per square inch of filter area | = | 1.4      | μg/in² |
| 2.54     | = conversion constant                            | = | 2.54     | cm/in  |
| 4        | = conversion constant                            | = | 4        |        |
| 3.141593 | = conversion constant (pi)                       | = | 3.141593 |        |
|          |  |   |          |        |
| Α        | = maximum front-half blank correction criteria   | = | 12.46    | пa     |

2. Allowable blank correction - combined front and back-half sample fractions (µg)

| $m_{FB-allow}$          | $= m_{FB}$ if $m_{FB} \le A + 1$                         |   |
|-------------------------|--|---|
| m <sub>FB - allow</sub> | $= MAX \left[ A + 1,  MIN \left( m_{FB} \right. \right)$ | $0.05 \times m_{FS}$ )] if $m_{FB} > A + 1$ |

| $m_{FB}$             | = phosphorus amount in combined front- and back-half blank   | = | 20.2065 | μg |
|----------------------|--|---|---------|----|
| $m_{FS}$             | = phosphorus amount in combined front- and back-half sample  | = | 46.9058 | μg |
| A+1                  | = max combined front- & back-half blank correction criteria  | = | 12.46   | μg |
| $0.05 \times m_{FS}$ | = 5% of combined front- and back-half sample amount          | = | 2.3453  | μg |
| MAX                  | = arithmetic operator that returns the maximum of two values |   |         |    |
| MIN                  | = arithmetic operator that returns the minimum of two values |   |         |    |

 $m_{FB-allow}$  = allowable combined Phosphorus blank correction = 12.4600  $\mu g$ 

NOTE: In this case, the second criteria applies.

3. Combined front- and back-half sample corrected for allowable blank  $(\mu g)$ 

$$m_n = m_{FS} - m_{FB-allow}$$

Where:

| $m_{FS}$              | = phosphorus amount in combined front- and back-half sample        | = | 46.9058 | μg |
|-----------------------|--|---|---------|----|
| $m_{\text{FB-allow}}$ | <ul> <li>allowable combined phosphorus blank correction</li> </ul> | = | 12.4600 | μg |
|                       |  |   |         |    |
| m <sub>n</sub>        | = blank-corrected phosphorus in combined sample                    | = | 34.4458 | μg |

# USEPA Method 5/29 (FPM/Metals) Phosphorus Sample Calculations

### Sample data taken from Run 1

Note: The tables presenting the results are generated electronically from raw data. It may not be possible to exactly duplicate these results using a calculator. The reference method data, results, and all calculations are carried to sixteen decimal places throughout. The final table is formatted to an appropriate number of significant figures.

101017 121607 P\_M

1. Phosphorus concentration (lb/dscf)

$$C_{sd} = \left(\frac{m_n}{V_{mstd}}\right) \left(\frac{2.205 \times 10^{-3}}{10^6}\right)$$

Where:

 $m_n$  = phosphorus collected in sample (total μg) = 34.4458 μg  $V_{mstd}$  = volume metered, standard (dscf) = 33.3002 dscf 2.205 x 10<sup>-3</sup> = conversion factor (lb/g) = 2.205E-03 lb/g 10<sup>6</sup> = conversion factor (μg/g) = 1.0E+06 μg/g

C<sub>sd</sub> = phosphorus concentration (lb/dscf) = 2.2809E-09 lb/dscf

2. Phosphorus concentration (µg/dscm)

$$C_{sd} = \left(\frac{m_n}{V_{mstd}}\right) (35.31)$$

Where:

 $m_n$  = phosphorus collected in sample (total μg) = 34.4458 μg  $V_{mstd}$  = volume metered, standard (dscf) = 33.3002 dscf 35.31 = conversion factor (dscf/dscm) = 35.31 dscf/dscm

 $C_{sd}$  = phosphorus concentration (µg/dscm) = 3.6525E+01 µg/dscm

3. Phosphorus concentration (mg/dscm)

$$C_{sd} = \left(\frac{m_n}{V_{mstd}}\right) \left(\frac{35.31}{1000}\right)$$

Where:

= phosphorus collected in sample (total µg)  $m_n$ 34.4458 μg  $V_{\text{mstd}}$ = volume metered, standard (dscf) 33.3002 dscf 35.31 = conversion factor (dscf/dscm) 35.31 dscf/dscm 1000 = conversion factor (µg/mg) 1000 µg/mg

C<sub>sd</sub> = phosphorus concentration (mg/dscm) = 3.6525E-02 mg/dscm

# 4. Phosphorus concentration (µg/Nm3 dry)

$$C_{sd} = \left(\frac{m_n}{V_{mstd}}\right) (35.31) \left(\frac{68 + 460}{32 + 460}\right)$$

# Where:

| $m_n$      | = phosphorus collected in sample (total μg) | = | 34.4458 | μg        |
|------------|---|---|---------|-----------|
| $V_{mstd}$ | = volume metered, standard (dscf)           | = | 33.3002 | dscf      |
| 35.31      | = conversion factor (dscf/dscm)             | = | 35.31   | dscf/dscm |
| 68         | = standard temperature (°F)                 | = | 68      | °F        |
| 32         | = normal temperature (°F)                   | = | 32      | °F        |
| 460        | = °F to °R conversion constant              | = | 460     |           |
|            |   |   |         |           |

= phosphorus concentration (µg/Nm3 dry)  $C_{\text{sd}}$  $= 3.9197E+01 \mu g/Nm^3 dry$ 

## 5. Phosphorus concentration at actual gas conditions (lb/acf example)

$$C_a = C_{sd} \left( \frac{Q_{std}}{Q_a} \right)$$

### Where:

| $egin{array}{l} C_{sd} \ Q_{std} \ Q_a \end{array}$ | <ul><li>= phosphorus concentration (lb/dscf)</li><li>= volumetric flow rate at standard conditions, dry basis (dscfm)</li><li>= volumetric flow rate at actual conditions (acfm)</li></ul> | =<br>=<br>= | 2.2809E-09<br>11,383<br>13,281 | lb/dscf<br>dscfm<br>acfm |
|---|--|-------------|--------------------------------|--------------------------|
| C <sub>a</sub>                                      | = phosphorus concentration at actual gas conditions (lb/acf)   | =           | 1.9550E-09                     | lb/acf                   |

6. Phosphorus emission rate (lb/hr) 
$$E_{lb/hr} = \left(\frac{m_n}{V_{mstd}}\right) \left(\frac{2.205 \times 10^{-3}}{10^6}\right) (Q_{std}) (60)$$

# Where:

| $m_n$                    | = phosphorus collected in sample (total µg)                      | = | 34.4458   | μg     |
|--------------------------|--|---|-----------|--------|
| $V_{mstd}$               | = volume metered, standard (dscf)                                | = | 33.3002   | dscf   |
| 2.205 x 10 <sup>-3</sup> | = conversion factor (lb/g)                                       | = | 2.205E-03 | lb/g   |
| 10 <sup>6</sup>          | = conversion factor (μg/g)                                       | = | 1.0E+06   | μg/g   |
| $Q_{std}$                | = volumetric flow rate at standard conditions, dry basis (dscfm) | = | 11,383    | dscfm  |
| 60                       | = conversion factor (min/hr)                                     | = | 60        | min/hr |
|                          |  |   |           |        |

 $E_{lb/hr}$ = phosphorus emission rate (lb/hr) 1.5578E-03 lb/hr

7. Phosphorus emission rate (g/s)

$$E_{g/s} = \left(\frac{m_n}{V_{mstd}}\right) \left(\frac{Q_{std}}{(10^6)(60)}\right)$$

Where:

| $m_n$            | = phosphorus collected in sample (total μg)                      | = | 34.4458 | μg      |
|------------------|--|---|---------|---------|
| $V_{mstd}$       | = volume metered, standard (dscf)                                | = | 33.3002 | dscf    |
| $Q_{\text{std}}$ | = volumetric flow rate at standard conditions, dry basis (dscfm) | = | 11,383  | dscfm   |
| 10 <sup>6</sup>  | = conversion factor (µg/g)                                       | = | 1.0E+06 | μg/g    |
| 60               | = conversion factor (sec/min)                                    | = | 60      | sec/min |

 $E_{g/s}$  = phosphorus emission rate (g/s) = 1.9625E-04 g/s

8. Phosphorus emission rate - Production-based (lb/unit)

$$E_{RP} = \left(\frac{m_n}{V_{mstd}}\right) \left(\frac{2.205 \times 10^{-3}}{10^6}\right) \left(\frac{(Q_{std})(60)}{R_p}\right)$$

Where:

| $m_n$                    | = phosphorus collected in sample (total μg)                      | = | 34.4458   | μg         |
|--------------------------|--|---|-----------|------------|
| $V_{mstd}$               | = volume metered, standard (dscf)                                | = | 33.3002   | dscf       |
| 2.205 x 10 <sup>-3</sup> | = conversion factor (lb/g)                                       | = | 2.205E-03 | lb/g       |
| 10 <sup>6</sup>          | = conversion factor (µg/g)                                       | = | 1.0E+06   | μg/g       |
| $Q_{std}$                | = volumetric flow rate at standard conditions, dry basis (dscfm) | = | 11,383    | dscfm      |
| 60                       | = conversion factor (min/hr)                                     | = | 60        | min/hr     |
| $R_p$                    | = production rate (units/hr)                                     | = | 323       | units/hour |
|                          |  |   |           |            |
| E <sub>RP</sub>          | = phosphorus emission rate - production-based (lb/xxxxx)         | = | #REF!     | lb/unit    |

9. Phosphorus emission rate - Production-based (g/unit)

$$E_{RP} = \left(\frac{m_{CPM}}{V_{mstd}}\right) \left(\frac{(Q_{std})(60)}{(10^6)(R_p)}\right)$$

Where:

| $m_n$           | = phosphorus collected in sample (total µg)                      | = | 30.8407 | μg         |
|-----------------|--|---|---------|------------|
| $V_{mstd}$      | = volume metered, standard (dscf)                                | = | 33.3002 | dscf       |
| 10 <sup>6</sup> | = conversion factor (µg/g)                                       | = | 1.0E+06 | μg/g       |
| $Q_{std}$       | = volumetric flow rate at standard conditions, dry basis (dscfm) | = | 11,383  | dscfm      |
| 60              | = conversion factor (min/hr)                                     | = | 60      | min/hr     |
| $R_p$           | = production rate (units/hr)                                     | = | 323     | units/hour |
|                 |  |   |         |            |

 $E_{RP}$  = phosphorus emission rate - production-based (g/xxxxx) = #REF! g/unit

Sims Metal Management CleanAir Project No. 13318 Johnston, RI TE Outlet

# **CEM Field Sample Calculations** for THC Stack Hi Range

# Sample data taken from Run 1 and Channel 4

Note: The tables presenting the results are generated electronically from raw data. It may not be possible to exactly duplicate these results using a calculator. The reference method data, results and all calculations are carried to sixteen decimal places throughout. The final table is formatted to an appropriate number of significant figures.

101917 132852

1. Average of a calibration series

$$C_{mce} = \frac{(C_1 + C_2 + C_3)}{3}$$

Where:

C<sub>1</sub>,C<sub>2</sub>,C<sub>3</sub> = concentrations of 3 consecutive gas samples that are representative of the calibration gas

C<sub>mce</sub> = average concentration of a calibration series = 146.556 ppmwv In this case the low cal series for channel 4

2a. Calibration Error Check for Hydrocarbons (5% of actual calibration gas value error allowed by Method 25A)

| $E_{{\scriptscriptstyle HC}}$<br>Where: | $= abs \left  \frac{C_{mce} - C_{ma}}{C_{ma}} \right  \le l_{cal}$                            |    |         |       |
|---|---|----|---------|-------|
| $C_{mce}$                               | = average concentration of a calibration series   | =  | 146.556 | ppmwv |
| $C_{ma}$                                | In this case the low cal series for channel 4 = concentration of actual calibration gas value | == | 150.000 | ppmwv |
| cal                                     | = limit for calibration error for hydrocarbons  | =  | 5.0%    |       |
| E <sub>HC</sub>                         | = calibration error check value   | =  | 2.30%   | Pass  |

2b. Calibration Error Check for non-Hydrocarbons (2% of Instrument Span)

$$E = abs \left| \frac{C_{mce} - C_{ma}}{Span} \right| \leq l_{cal}$$
 Where:
$$C_{mce} = \text{average concentration of a calibration series} = 146.556 \quad \text{ppmwv}$$
 In this case the low cal series for channel 4
$$C_{ma} = \text{concentration of actual calibration gas value} = 150.000 \quad \text{ppmwv}$$
 Span = instrument span value = 1000.000 |
$$l_{cal} = \text{limit for calibration error for non-hydrocarbons} = 2.0\%$$

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3. System Bias as Percent of Span Value (5% is allowed)

$$E_{Bias} = abs \left| \frac{C_{mf} - C_{mce}}{Span} \right| \le l_{bias}$$

Where:

| $C_{mce}$         | <ul> <li>average concentration of a calibration series</li> <li>in this case the High cal series for channel 4</li> </ul> | = | 861.562  | ppmwv |
|-------------------|---|---|----------|-------|
| $C_{mf}$          | = calibration error response concentration for Cal01  |   | 854.099  | ppmwv |
| Span              | = instrument span value   | = | 1000.000 | ppmwv |
| l <sub>bias</sub> | = limit for system bias error   | = | 5.0%     |       |
| E <sub>bias</sub> | = calibration bias error check value  | = | 0.75%    | Pass  |

4. System Drift as Percent of Span Value (3%)

$$E_{Drift} = abs \left| \frac{C_{mf} - C_{mi}}{Span} \right| \le l_{drift}$$

Where:

| C <sub>mi</sub><br>Span                  | = calibration error response concentration for Cal00 (initial) = instrument span value         | = | 861.562<br>1000.000 | ppmwv |
|--|--|---|---------------------|-------|
| l <sub>drift</sub><br>E <sub>drift</sub> | <ul><li>= limit for system drift error</li><li>= calibration drift error check value</li></ul> | = | 3.0%<br>0.75%       | Pass  |

5. Average Concentration for an entire Run

$$C = \frac{\sum_{i=1}^{N} C_{i}}{N}$$

Where: i=1  $C_i$  = All concentration readings for the entirety of Run 1 = 0.830 ppmwv for the monitor looking for THC on channel 4 N = total number of readings in Run 1 = 95 C = average THC concentration for Run 1 = 455.716 ppmwv

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6. Drift-Corrected Average Concentration for an entire Run

$$C_{DC} = \left(C - \frac{C_{oi} + C_{of}}{2}\right) \left(\frac{C_{ma}}{\frac{C_{mi} + C_{mf}}{2} - \frac{C_{oi} + C_{of}}{2}}\right)$$

| $C_{ma}$        | = concentration of actual calibration gas value   | =     | 861.000 | ppmwv |
|-----------------|---|-------|---------|-------|
| С               | = average THC concentration for Run 1   | =     | 455.716 | ppmwv |
| $C_{mf}$        | = calibration error response concentration for Cal01 (final)                                      | =     | 854.099 | ppmwv |
| $C_{mi}$        | = calibration error response concentration for Cal00 (initial)                                    | =     | 861.562 | ppmwv |
| $C_{of}$        | <ul> <li>calibration error response concentration for Cal01 (final)<br/>for zero gas</li> </ul>   | ***** | 1.214   | ppmwv |
| C <sub>oi</sub> | <ul> <li>calibration error response concentration for Cal00 (initial)<br/>for zero gas</li> </ul> | =     | -0.451  | ppmwv |
| $C_{DC}$        | = drift corrected average concentration for Run 1   | =     | 457.221 | ppmwv |

Sims Metal Management CleanAir Project No. 13318 Johnston, RI TE Outlet

# CEM Emissions Sample Calculations for THC Stack Hi Range

# Sample data taken from Run 1 and Channel 4

457.221

ppmwv

Note: The tables presenting the results are generated electronically from raw data. It may not be possible to exactly duplicate these results using a calculator. The reference method data, results and all calculations are carried to sixteen decimal places throughout. The final table is formatted to an appropriate number of significant figures.

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# 1. THC concentration (ppmdv)

$$C(ppmdv) = k_1 \times C_{DC} \qquad if \qquad dry \qquad gas$$
 
$$C(ppmdv) = \frac{k_1 \times C_{DC}}{\left(1 - \frac{B_W}{100}\right)} \qquad if \qquad wet \qquad gas$$
 Where:

| $C_{DC}$       | = drift corrected average concentration             | = | 457.221 | ppmwv |
|----------------|---|---|---------|-------|
| $B_w$          | = actual water vapor in gas (% v/v)                 | = | 7.350   | % v/v |
| 100            | = conversion factor to change percentage to decimal | = | 100     |       |
| k <sub>1</sub> | = ppm/% to ppm conversion factor for diluent gases  | = | 1       |       |
|                |   |   |         |       |

C (ppmdv) = THC concentration (ppmdv) = 493.490 ppmdv

### 2. THC concentration (ppmwv)

$$C(ppmwv) = k_1 \times C_{DC} \qquad if \qquad wet \qquad gas$$
 
$$C(ppmwv) = k_1 \times C_{DC} \times \left(1 - \frac{B_W}{100}\right) \qquad if \qquad dry \qquad gas$$

= THC concentration (ppmwv)

## Where:

C (ppmwv)

| $C_{DC}$       | = drift corrected average concentration             | = | 457.221 | ppmwv |
|----------------|---|---|---------|-------|
| $B_w$          | = actual water vapor in gas (% v/v)                 | = | 7.350   | % v/v |
| 100            | = conversion factor to change percentage to decimal | = | 100     |       |
| k <sub>1</sub> | = ppm/% to ppm conversion factor for diluent gases  | = | 1       |       |
|                |   |   |         |       |

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3. THC concentration (lb/dscf)

$$C(lb/dscf) = \frac{C(ppmdv) \times MW(gas)}{10^{6} ppm \times 385.3}$$

Where:

C (ppmdv) = THC concentration (ppmdv) = 493.490 ppmdv MW = Molecular Weight of THC gas = 44.0972 lb/lb-mole

 $10^6$  = conversion factor from decimal to ppm = 1.00E+06

385.3 = molar volume = 385.3 dscf/lb-mole

C (lb/dscf) = THC concentration (lb/dscf) = 5.648E-05 lb/dscf

4. THC concentration (lb/scf)

$$C(lb / scf)$$
 =  $C(lb / dscf) \times \frac{Q_{std}}{Q_{std}}$ 

Where:

C (lb/scf) = THC concentration (lb/scf) = 5.233E-05 lb/scf

5. THC concentration (lb/acf)

$$C(lb / acf)$$
 =  $C(lb / dscf) \times \frac{Q_{std}}{Q_a}$ 

Where:

C (lb/acf) = THC concentration (lb/acf) = 4.841E-05 lb/acf

6. THC concentration (%dv)

$$C(\% dv) = C(ppmdv) \times \frac{100}{10^6}$$

Where:

C (ppmdv) = THC concentration (ppmdv) = 493.490 ppmdv 100 = conversion factor from decimal to percentage = 1.00E+02

100 = conversion factor from decimal to percentage = 1.00E+02 10<sup>6</sup> = conversion factor from decimal to ppm = 1.00E+06

C (%dv) = THC concentration (%dv) = 0.0493% %dv

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7. THC concentration (mg/dscm)

$$C(mg/dscm) = C(lb/dscf) \times k_2 \times 35.31$$

### Where:

C (lb/dscf) = THC concentration (lb/dscf) 5.648E-05 lb/dscf  $k_2$ = conversion factor from lb to mg 453515 mg/lb 35.31 = conversion factor from dscf to dscm 35.31 ft<sup>3</sup>/m<sup>3</sup>

C (mg/dscm) = THC concentration (mg/dscm) 904.440 mg/dscm

# 8. THC concentration (mg/Nm3 dry)

$$C \qquad (mg / Nm^3 dry) \qquad = C(lb / dscf) \times k_2 \times 35.31 \times \left(\frac{68 + 460}{32 + 460}\right)$$

### Where:

| C (lb/dscf)<br>k <sub>2</sub> | <ul><li>THC concentration (lb/dscf)</li><li>conversion factor from lb to mg</li></ul> | = | 5.648E-05<br>453515 | lb/dscf<br>mg/lb                |
|-------------------------------|---|---|---------------------|---------------------------------|
| 35.31                         | = conversion factor from dscf to dscm   | = | 35.31               | ft <sup>3</sup> /m <sup>3</sup> |
| 68                            | = standard temperature (°F)   | = | 68                  | °F                              |
| 32                            | = normal temperature (°F)   | = | 32                  | °F                              |
| 460                           | = °F to °R conversion constant  | = | 460                 |                                 |

C (mg/Nm3 dr = THC concentration (mg/Nm3 dry) mg/Nm<sup>3</sup> dry 970.619

## 9. THC emission rate (lb/hr)

$$E_{lb/hr} = C(lb/dscf) \times Q_{std} \times 60$$

### Where:

| C (lb/dscf)<br>Q <sub>std</sub> | <ul><li>= THC concentration (lb/dscf)</li><li>= volumetric flow rate at standard conditions, dry basis (dscfm)</li></ul> | = | 5.648E-05<br>11383.24205 | lb/dscf<br>dscfm |
|---------------------------------|--|---|--------------------------|------------------|
| 60                              | = conversion factor (min/hr)   | = | 60                       | min/hr           |
| E <sub>lb/hr</sub>              | = THC emission rate (lb/hr)  | = | 38.575                   | lb/hr            |

# 10. THC emission rate (kg/hr)

$$E_{kg/hr} = C(lb/dscf) \times Q_{std} \times 60 \times 0.454$$

# Where:

| C (lb/dscf)        | = THC concentration (lb/dscf)                                    | = | 5.648E-05   | lb/dscf |
|--------------------|--|---|-------------|---------|
| $Q_{std}$          | = volumetric flow rate at standard conditions, dry basis (dscfm) | = | 11383.24205 | dscfm   |
| 60                 | = conversion factor (min/hr)                                     | = | 60          | min/hr  |
| 0.454              | = conversion factor (kg/lb)                                      | = | 0.454       | kg/lb   |
|                    |  |   |             |         |
| E <sub>ka/hr</sub> | = THC emission rate (kg/hr)                                      | = | 17.494      | ka/hr   |

Prepared by Clean Air Engineering Proprietary Software

SS CEM Version 06-2004g5

### CleanAir Project No. 13318

### Johnston, RI

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### 11. THC emission rate (gm/sec)

$$E_{gm/sec} = C(lb/dscf) \times Q_{std} \times \frac{454}{60}$$

Where:

C (lb/dscf) = THC concentration (lb/dscf) 5.648E-05 lb/dscf = volumetric flow rate at standard conditions, dry basis (dscfm) = Q<sub>std</sub> 11383.24205 dscfm 60 = conversion factor (sec/min) 60 sec/min 454 = conversion factor (q/lb) 453.515 kg/lb = THC emission rate (gm/sec) E<sub>om/sec</sub> 4.860 gm/sec

# 12. THC Fd-based emission rate (ng/J)

$$E_{\mathit{Fd}} = C (\mathit{lb} \, / \, \mathit{dscf} \,) \times \left(4.54 \times 10^{11}\right) \times F_{\mathit{d}} \times \left(9.486 \times 10^{-10}\right) \times \left(\frac{20}{20.9}\right) \times \left(\frac{10}{20.9}\right) \times \left(\frac{20}{20.9}\right) \times \left(\frac{2$$

 $9.486*10^{-10}$  = conversion factor (MMBtu/J) = 9.486E-10 MME  $O_2$  = proportion of oxygen in the gas stream by volume (%) = 20.963 % 20.9 = oxygen content of ambient air (%) = 20.9 %

 $E_{Fd}$  = THC Fd-based emission rate (ng/J) = 0.000 ng/J

# 13. THC production-based emission rate (lb/unit)

$$E_{RP} = C(lb / dscf) \times Q_{std} \times \frac{60}{R_{p}}$$

Where:

C (lb/dscf) = THC concentration (lb/dscf) 5.648E-05 lb/dscf  $Q_{std}$ = volumetric flow rate at standard conditions, dry basis (dscfm) = 11383.24205 dscfm 60 = conversion factor (min/hr) 60 min/hr  $R_p$ = production rate (units/hr) 323.04 units/hour

E<sub>RP</sub> = THC production-based emission rate (lb/unit) = 1.194E-01 lb/unit

### 14. THC production-based emission rate (kg/unit)

$$E_{RP} = C \left( lb / dscf \right) \times 0.454 \times Q_{std} \times \frac{60}{R_{p}}$$

Where:

C (lb/dscf) = THC concentration (lb/dscf) 5.648E-05 lb/dscf 0.454 = conversion factor (kg/lb) 0.454 kg/lb  $Q_{std}$ = volumetric flow rate at standard conditions, dry basis (dscfm) = 11383.24205 dscfm = conversion factor (min/hr) 60 min/hr  $R_p$ = production rate (units/hr) 323.04 units/hour

E<sub>RP</sub> = THC production-based emission rate (kg/unit) = 5.416E-02 kg/unit

### USEPA METHOD TO-15 SAMPLE CALCULATIONS - Chlorodifluoromethane Results

### Sample data taken from Run 1

3.1594

ppmwv

Note: The tables presenting the results are generated electronically from raw data. It may not be possible to exactly duplicate these results using a calculator. The reference method data, results and all calculations are carried to sixteen decimal places throughtout. The final table is formatted to an appropriate number of significant figures.

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1. Conversion of as-measured Chlorodifluoromethane concentration to ppm calculation basis

$$C_{s(ppm)} = C_{meas} \times k_1$$

Where:

= average concentration measured , (ppbdv) Cmeas 3410.0000 ppbdv = conversion factor to convert measured concentration to ppm 0.0010

C<sub>s (ppm)</sub> = Chlorodifluoromethane concentration, dry basis (ppmdv) 3.4100 ppmdv

2. Chlorodifluoromethane concentration, wet basis (ppmwv)

$$C_{sw(ppn)} = C_{s(ppn)} \left( 1 - \frac{B_w}{100} \right)$$

Where:

C<sub>sw (ppm)</sub>

= Chlorodifluoromethane concentration, dry basis (ppmdv) C<sub>s (ppm)</sub> 3.4100 ppmdv = actual water vapor in gas (% v/v) % v/v 7.3496 100 = conversion factor (%) 100 % \_\_\_ = Chlorodifluoromethane concentration, wet basis (ppmwv)

3. Chlorodifluoromethane concentration (lb/dscf)

$$C_{sd (lb/dsef)} = \frac{C_{sd (ppmdv)} \times MW}{10^6 ppm \times 385.3}$$

Where:

= average concentration measured using field GC, dry basis 3.4100 ppmdv C<sub>sd (ppmdv)</sub> MW = molecular weight of Chlorodifluoromethane (g/g-mole) 86.470 g/g-mole 385.3 = molar gas volume (dscf/lb-mole) 385.3 dscf/lb-mole

C<sub>sd</sub> (lb/dscf) = Chlorodifluoromethane concentration (lb/dscf) 7.6528E-07 lb/dscf

# 4. Chlorodifluoromethane concentration (mg/dscm)

$$C_{sd (mg / dscm)} = C_{sd (lb / dscf)} \times (453.515)(1000)(35.31)$$

### Where:

| C <sub>sd (lb/dscf)</sub> | = Chlorodifluoromethane concentration (lb/dscf) | = | 7.6528E-07 | lb/dscf   |
|---------------------------|---|---|------------|-----------|
| 453.515                   | = conversion factor (gm/lb)                     | _ | 453.515    | gm/lb     |
| 1000                      | = conversion factor (mg/gm)                     | = | 1000       | mg/gm     |
| 35.31                     | = conversion factor (dscf/dscm)                 | = | 35.31      | dscf/dscm |
|                           |   |   |            |           |

 $C_{sd (mg/dscm)}$  = Chlorodifluoromethane concentration (mg/dscm) = 12.2549 mg/dscm

# 5. Chlorodifluoromethane concentration (mg/Nm3 dry)

$$C_{sd(mg/Nm^3)} = C_{sd(lb/dscf)} (453.415)(1000)(35.31) \left(\frac{68+460}{32+460}\right)$$

### Where:

| C <sub>sd (lb/dscf)</sub> | = Chlorodifluoromethane concentration (lb/dscf) | NAME . | 7.6528E-07 | lb/dscf   |
|---------------------------|---|--------|------------|-----------|
| 453.515                   | = conversion factor (gm/lb)                     | =      | 453.515    | gm/lb     |
| 1000                      | = conversion factor (mg/gm)                     | ==     | 1000       | mg/gm     |
| 35.31                     | = conversion factor (dscf/dscm)                 | =      | 35.31      | dscf/dscm |
| 68                        | = standard temperature (°F)                     | =      | 68         | °F        |
| 32                        | = normal temperature (°F)                       | =      | 32         | °F        |
| 460                       | = °F to °R conversion constant                  | =      | 460        | °F        |
|                           |   |        |            |           |

 $C_{sd (mg/Nm3)}$  = Chlorodifluoromethane concentration (mg/Nm3 dry) = 10.5041 mg/Nm<sup>3</sup> dry

# 6. Chlorodifluoromethane concentration at actual gas conditions (lb/acf example)

$$C_a = C_{sd} \left( \frac{Q_{std}}{Q_a} \right)$$

### Where:

| $C_{\sf sd}$     | = Chlorodifluoromethane concentration (lb/dscf)                  | = | 7.6528E-07 | lb/dscf |
|------------------|--|---|------------|---------|
| $Q_{\text{std}}$ | = volumetric flow rate at standard conditions, dry basis (dscfm) | = | 11,383     | dscfm   |
| $Q_a$            | = volumetric flow rate at actual conditions (acfm)               | = | 13,281     | acfm    |
|                  |  |   |            |         |

C<sub>a</sub> = Chlorodifluoromethane concentration at actual gas conditions ( = 6.5595E-07 lb/acf

# 7. Chlorodifluoromethane rate (lb/hr)

$$E_{lb/hr} = C_{sd(lb/dscf)} \times Q_{std} \times 60$$

## Where:

| C <sub>sd (lb/dscf)</sub> | = Chlorodifluoromethane concentration (lb/dscf)                  | = | 7.6528E-07 | lb/dscf |
|---------------------------|--|---|------------|---------|
| $Q_{std}$                 | = volumetric flow rate at standard conditions, dry basis (dscfm) | = | 11,383     | dscfm   |
| 60                        | = conversion factor (min/hr)                                     | = | 60         | min/hr  |
| E <sub>lb/hr</sub>        | = Chlorodifluoromethane rate (lb/hr)                             | = | 0.5227     | lb/hr   |

8. Chlorodifluoromethane rate (kg/hr) 
$$E_{\it kg/hr} = C_{\it sd(lb/dscf)} \times Q_{\it sd} \times 60 \times \left(\frac{453.515}{1000}\right)$$

### Where:

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| • |                           |  |   |            |         |
|---|---------------------------|--|---|------------|---------|
|   | C <sub>sd (lb/dscf)</sub> | = Chlorodifluoromethane concentration (lb/dscf)                  | = | 7.6528E-07 | lb/dscf |
|   | $Q_{std}$                 | = volumetric flow rate at standard conditions, dry basis (dscfm) | = | 11,383     | dscfm   |
|   | 60                        | = conversion factor (min/hr)                                     | = | 60         | min/hr  |
|   | 453.515                   | = conversion factor (gm/lb)                                      | = | 453.515    | gm/lb   |
|   | 1000                      | = conversion factor (mg/gm)                                      | = | 1000       | mg/gm   |
|   |                           |  |   |            |         |
|   | E <sub>kg/hr</sub>        | = Chlorodifluoromethane rate (kg/hr)                             | = | 0.2370     | kg/hr   |

#REF! Chlorodifluoromethane rate - Production-based (lb/unit)

$$E_{RP} = C_{sd (lb / dscf)} \times \left( \frac{Q_{std} \times 60}{R_{p}} \right)$$

### Where:

| C <sub>sd (lb/dscf)</sub> | = Chlorodifluoromethane concentration (lb/dscf)                  | = | 7.6528E-07 | lb/dscf    |
|---------------------------|--|---|------------|------------|
| $Q_{std}$                 | = volumetric flow rate at standard conditions, dry basis (dscfm) | = | 11,383     | dscfm      |
| 60                        | = conversion factor (min/hr)                                     | = | 60         | min/hr     |
| $R_p$                     | = production rate (units/hr)                                     | = | 323.04     | units/hour |
|                           |  |   |            |            |
| $E_RP$                    | = Chlorodifluoromethane rate - production based(lb/xxxx)         | = | 1.6180E-03 | lb/unit    |

#REF! Chlorodifluoromethane rate - Production-based (kg/unit)

$$E_{RP} = C_{sd(lb/dscf)} \times \left( \frac{Q_{std} \times 60 \times 453.515}{1000 \times R_p} \right)$$

### Where:

| C <sub>sd (lb/dscf)</sub> | = Chlorodifluoromethane concentration (lb/dscf)                  | = | 7.6528E-07 | lb/dscf    |
|---------------------------|--|---|------------|------------|
| $Q_{std}$                 | = volumetric flow rate at standard conditions, dry basis (dscfm) | = | 11,383     | dscfm      |
| 60                        | = conversion factor (min/hr)                                     | = | 60         | min/hr     |
| 453.515                   | = conversion factor (gm/lb)                                      | = | 453.515    | gm/lb      |
| 1000                      | = conversion factor (mg/gm)                                      | = | 1000       | mg/gm      |
| $R_p$                     | = production rate (units/hr)                                     | = | 323.04     | units/hour |
|                           |  |   |            |            |
| E <sub>RP</sub>           | = Chlorodifluoromethane rate - production based(kg/xxxx)         | = | 7.3379E-04 | kg/unit    |

